

# **UNITED STATES PATENT APPLICATION**

**TITLE:** PROCESS AND SYSTEM FOR THE CONDENSATION OF MULTI-COMPONENT WORKING FLUIDS

**INVENTOR:** Alexander I. Kalina

**ASSIGNEE:** KALEX, LLC.

## **BACKGROUND OF THE INVENTION**

### **1. Field of the Invention**

[0001] The present invention relates to a process and system for condensing a multi-component fluid, where the process and system are designed to provide a substantial increase in a heat transfer coefficient during condensation of multi-component fluids resulting in a drastic reduction in size and cost of heat exchangers need to condense such fluids.

[0002] More particularly, the present invention relates to a process and system for condensing a multi-component fluid, where the process and system are designed to provide a substantial increase in a heat transfer coefficient during condensation of multi-component fluids resulting in a drastic reduction in size and cost of heat exchange units need to condense the fluids and includes at least two heat transfer stages and at least one scrubber interconnected so that streams are split and mixed in such a way as to increase the heat transfer coefficient in each heat exchange unit.

### **2. Description of the Related Art**

[0003] The condensation of multi-component working fluids is widely used in the chemical, petrochemical, refrigeration and power industries. It is important to note that the efficacy of this process is substantially lower than the efficacy of condensation of pure, single component fluids. In the process of condensation of single component fluids, the only thermal resistance is the thermal resistance of the film of condensate that covers the cooling surface. The temperature of this film is the same as the temperature of the whole condensing stream and therefore the temperature difference across the film of condensate is equal to the temperature difference between the temperature of the condensing steam and the temperature of the cooling surface.

[0004] In distinction to the process of the condensation of single component fluid, the process of condensing multi-component fluids occurs at variable temperatures and includes distinct sub-processes which occur simultaneously. Condensation occurs on a cooling surface which is covered by a film of condensate. Vapor which is not yet condensed is absorbed by this the surface of this film of condensate. The remaining non-condensed, portion of vapor is cooled by the surface of the film of condensate. In turn, the film of condensate is cooled by the cooling surface. The entire

stream of heat removed from the fluid is therefore passing through the film of condensate, whereas only a portion of this stream, *i.e.*, heat released in phase change and sensible heat released in the cooling of the vapor, is transferred to the surface of the film. Therefore, there is always a temperature difference between the vapor and the film of condensate as well as a temperature difference between the film of condensate and the cooling surface.

[005] If, in any cross-section of a heat exchanger, the vapor and liquid would be thoroughly mixed so that they would be in complete equilibrium, then the mixture of liquid and vapor would have a temperature which is referred to as a "mixed mean temperature", hereafter referred to as  $t_{mm}$ . It is clear that the temperature of the vapor  $t''$  is always higher than  $t_{mm}$ , whereas the temperature of the film  $t'$  is always lower than  $t_{mm}$ . As a result, the driving force for transferring heat through the film of condensate, *i.e.*, temperature difference in between the film and cooling surface, is reduced and the heat transfer coefficient is reduced as well.

[006] It is clear that in the initial stages of condensation, when the condensing stream consists mostly of vapor, the temperature of the film of condensate is substantially lower than  $t_{mm}$ , whereas the temperature of the vapor  $t''$  is close to  $t_{mm}$ . As a consequence of the temperature difference  $\Delta T$  across the film is substantially reduced and the heat transfer coefficient is drastically reduced. On the contrary, in the final stages of condensation, where the greater part of stream is already in the form of a condensate, the temperature of the condensate  $t'$  is close to  $t_{mm}$  whereas the temperature of the vapor is substantially higher than  $t_{mm}$ . In this case, the temperature difference  $\Delta t$  across the film and the heat transfer coefficient are only insignificantly reduced as compared to the condensation of single component fluids.

[0007] Thus, there is a need in the art for an apparatus and method using the apparatus for condensing a multi-component fluid while maximizing the heat transfer coefficient during the entire condensing process.

### **SUMMARY OF THE INVENTION**

[0008] The present invention provides a system for condensing multi-component fluids including at least two heat exchange stages and at least one scrubber, where the heat exchange stages and the at least one scrubber are interconnected so that streams are split and mixed in such a way as to increase the heat transfer coefficient in each of the heat exchange stages.

[0009] The present invention also provides a system for condensing multi-component fluids including a plurality of heat exchange stages and at least one scrubber, where the heat exchange stages and the at least one scrubber are interconnected so that streams are split and mixed in such

a ways as to increase the heat transfer coefficient in each of the heat exchange stages.

[0010] The present invention a plurality of heat exchange stages and a plurality of scrubbers, where the heat exchange stages and the scrubbers are interconnected so that streams are split and mixed in such a ways as to increase the heat transfer coefficient in each of the heat exchange stages.

[0011] The present invention provides a process for condensing multi-component fluids including the steps of feeding an input vapor stream comprising a multi-component fluid to a condensation system of this invention where it is split into two sub-streams, one being forwarded to a lower port of a scrubber and the second being combined with a liquid stream from a bottom port of the scrubber. The combined stream is then passes through a first heat exchanger where it is fully condensed forming a first condensed stream which is in turn splitter into two sub-streams, one being forwarded to a top port of the scrubber and the second sub-stream being combined with a scrubber vapor stream taken from an upper port of the scrubber to form a second combined stream. The second combined stream is then passes through a second heat exchanger where it is fully condensed forming a final liquid stream comprising a multi-component stream having a compositions the same or substantially the same as the input stream. The scrubber and its associated streams are designed to increase condensation efficiency by optimizing or maximizing a heat transfer coefficient in each heat exchanger.

[0012] The present invention also provides a condensation process including three or more heat exchangers where scrubber vapor streams are combined with condensed streams and optionally liquid streams are sent to or pulled from the scrubber. The scrubber and its associated streams are designed to increase condensation efficiency by optimizing or maximizing a heat transfer coefficient in each heat exchanger.

### **DESCRIPTION OF THE DRAWINGS**

[0013] The invention can be better understood with reference to the following detailed description together with the appended illustrative drawings in which like elements are numbered the same:

[0014] Figure 1 depicts a schematic diagram of a preferred embodiment of a system of this invention including two heat exchangers and one scrubber;

[0015] Figure 2 depicts a schematic diagram of another preferred embodiment of a system of this invention including three heat exchangers and one scrubber;

[0016] Figure 3 depicts a schematic diagram of another preferred embodiment of a system of this invention including three heat exchangers and one scrubber;

[0017] Figure 4 depicts a schematic diagram of another preferred embodiment of a system of this

invention including four heat exchangers and one scrubbers;

[0018] Figure 5 depicts a schematic diagram of another preferred embodiment of a system of this invention including three heat exchangers and two scrubbers; and

[0019] Figure 6 depicts a schematic diagram of a preferred embodiment of a heat extraction system of this including a condensing stage of this invention, a vaporization stage and an energy extraction stage.

### **DETAILED DESCRIPTION OF THE INVENTION**

[0020] The inventors have found that a superior apparatus, system and method using the apparatus can be constructed to condense a vaporized multi-component fluid while maintaining a maximized value of a heat transfer coefficient in each heat exchange stage. The apparatus includes at least two heat exchange stages, at least one scrubber, mixer valves and splitter valves for mixing and splitting streams, where vapor, liquid or mixed streams are removed and/or added to each heat exchange stage from the scrubbers or upstream heat exchange stages to provide a fully condensed multi-component fluid having substantially a same composition as the vaporized multi-component input fluid, while maximizing a heat transfer coefficient at each heat exchange stage.

[0021] The invention broadly relates to an apparatus/system for condensing multi-component fluids including at least two heat exchange stages and at least one scrubber unit. The apparatus further includes mixers, splitters, ports and lines configured so that a first portion of a multi-component vapor stream enters a multi-component vapor stream input port of the scrubber unit and a second portion of the multi-component vapor stream is mixed with a first liquid stream from a bottom output port of the scrubber unit. The mixed stream is then forwarded to an input of a first heat exchange stage, and a condensed stream exits through an output port of the first heat exchange stage. A portion of the condensed stream is forwarded to a top input port of the scrubber unit, while the remainder of the condensed stream is mixed with a vapor stream from a vapor output port of the scrubber. That mixed stream is then forwarded to an input of a second heat exchange stage where the stream is fully condensed exiting through an output port of the second heat exchange stage to form a fully condensed multi-component fluid having a composition substantially identical to the composition of the vapor multi-component input fluid. When additional heat exchange stages are incorporated into the apparatus, the output stream from each successive heat exchange stage can optionally either be split forwarding a portion of the output stream to secondary liquid input ports of the scrubber unit or mixed with secondary liquid streams from secondary liquid output ports of the scrubber unit. The resulting streams are then mixed with secondary vapor streams from

secondary vapor ports of the scrubber unit which are then fed into an input port of the next heat exchange stage. When additional scrubber units are incorporated into the apparatus, the scrubber units are associated with one or more of the heat exchange units.

[0022] The system and process of this invention allows a performance of condensation of multi-component fluids to occur in such a way that in every part of the process, the performance has an efficiency substantially identical to an efficiency of a final, most efficient stage of condensation, *i.e.*, has an efficiency substantially identical to an efficient of condensing a single component fluid.

[0023] The system and method includes a plurality of heat exchangers and at least one scrubber and splitters and mixers supporting streams that allow a mixed stream to be supplied to each heat exchange unit having parameters designed to increase, optimize or maximize the heat transfer coefficient in each heat exchanger. Condensation efficiency is greatly reduced if significant vapor is in contact with the heat exchange surfaces in the heat exchangers, while condensation efficiency is greatly increased if liquid is in contact with the heat exchange surfaces. The present invention is designed to ensure that each stream going into each heat exchanger has sufficient liquid content to that the heat exchange process is mediated primarily if not exclusively by liquid. The arrangement is especially critical for multi-component fluid because the boiling point to the fluid is continuously changing in the heat exchanger because the composition of the fluid is continuously changing.

[0024] In the following detailed description of the preferred embodiments of this invention as illustrated by the Figures, the heat exchange stages are shown a heat exchangers. However, the heat exchange stages can be any conventional or yet to be invented unit that can extract thermal energy from a vapor stream and cooling it to a point below its boiling point. Although no cooling stream is shown in the heat exchangers one of ordinary skill in the art will understand that the stream to be condensed is in thermal contact with a stream of fluid that is capable of lowering the temperature of the stream to be condensed as the stream passes through the heat exchanger. The stream of fluid can be liquid or gas or a mixture thereof and can be external or internal to the power plant in which such a condensation unit is utilized.

## **DETAILED DESCRIPTION OF THE DRAWINGS**

### **Detailed Description of Single Scrubber Embodiments**

#### **Two Heat Exchange Stages - One Scrubber**

[0025] Referring now to **Figure 1**, a preferred embodiment of an apparatus/system for condensing a multi-component fluid, generally **100**, is shown to comprise two heat exchange stages **102** and

104, including heat exchangers **HE1** and **HE2**, respectively. The system 100 also includes a scrubber **SC1**. An input vapor stream 110 comprising a multi-component fluid (the stream to be condensed) and having initial parameters as at a point 21, which can correspond to a state of saturated vapor, enters the system 100. The stream 110 is divided into two sub-streams 112 and 114, having parameters as at points 2 and 3, respectively at a first stream splitter 116. The sub-stream 112 having the parameters as at the point 2 is mixed with a first liquid stream 118 having parameters as at a point 4 at a first stream mixer 120. The state of liquid in the first liquid stream 118 having the parameters as at the point 4 corresponds to a state of saturated liquid, which is in equilibrium with the saturated vapor sub-stream 112 having the parameters as at the point 2. As a result of mixing, a first mixed stream 122 having parameters as at a point 5 is formed. The first mixed stream 122 having the parameters as at the point 5 passes through the heat exchanger **HE1** where it is fully condensed and exits the heat exchanger **HE1** as a first condensed stream 124 having parameters as at a point 6. The first condensed stream 124 having the parameters as at the point 6 corresponds to a state of saturated liquid and has a substantially leaner composition (*i.e.*, a substantially lower concentration of a low-boiling component of the multi-component fluid) than the input vapor stream 110.

[0026] Thereafter, the first condensed stream 124 having the parameters as at the point 6 is divided into two liquid sub-streams 126 and 128, having parameters as at points 8 and 9, respectively at a second splitter 130. Thereafter, the liquid sub-stream 128 having the parameters as at the point 9 is mixed with a scrubber vapor stream 132 having parameters as at a point 10 at a mixer 134, creating a second mixed stream 136 having parameters as at a point 11. The composition of the second mixed stream 136 having the parameters as at the point 11 is substantially the same as the composition of the stream 110 having the parameters as at the point 1. The stream 136 having the parameters as at the point 11 passes through the heat exchanger **HE2**, where it is fully condensed to form a liquid output stream 138 having parameters as at a point 12 corresponding to a state of saturated liquid.

[0027] The vapor sub-stream 114 having the parameters as at the point 3 (as described above) is forwarded to a lower port 140 of the scrubber **SC1**, while the liquid stream 126 having the parameters as at the point 8 is sent into a top port 142 of the scrubber **SC1**. A counter flow process of mass and heat exchange occurs in the scrubber **SC1**, where liquid flows down the scrubber **SC1** as vapor raises up. As a result, at the top of the scrubber **SC1**, vapor is in equilibrium with liquid having the parameters as at the point 10, which was sent to the top port 142 of the scrubber **SC1** (as

described above). This vapor is removed from an upper port 144 of the scrubber SC1, forming the vapor stream 132 having the parameters as at the point 10, which is mixed with the stream 128 having the parameters as at the point 9 (as described above). Liquid collected at the bottom of the scrubber SC1 is in equilibrium with vapor of the sub-stream 114 having the parameters as at the point 3 (as described above). That liquid is removed from a bottom port 146 of the scrubber SC1 forming the stream 118 having the parameters as at the point 4, which is mixed with the vapor stream 112 having the parameters as at the point 2 forming the mixed stream 122 having the parameters as at the point 5 (as described above).

[0028] The system is closed save for the input stream 110 and the output stream 138. Of course, when this condensing apparatus comprises a part of a complete energy extraction unit, the entire system is closed, *i.e.*, a multi-component fluid is sent through of vaporizing unit, then to an energy extraction unit and then to a fluid condensation unit of this invention and then back to the vaporizing unit forming a closed loop.

### **Three Heat Exchange Stages - One Scrubber - First Embodiment**

[0029] Referring now to **Figure 2**, a preferred embodiment of a system for condensing a multi-component fluid, generally 200, is shown to comprise three heat exchange stages 202, 204, and 206, each stage including a heat exchanger HE1, HE2, and HE3, respectively. The system also includes a scrubber SC1. An input vapor stream 210 comprising a multi-component fluid (the stream to be condensed) and having initial parameters as at a point 21, which can correspond to a state of saturated vapor, enters the system 200. The stream 210 is divided into vapor two sub-streams 212 and 214, having parameters as at points 22 and 23, respectively, at a splitter 216. The first vapor sub-stream 212 having the parameters as at the point 22 is mixed with a first liquid stream 218 having parameters as at a point 24 at a mixer 220. The state of liquid in the first liquid stream 218 having the parameters as at the point 24 corresponds to a state of saturated liquid, which is in equilibrium with the saturated vapor sub-stream 212 having parameters as at the point 22. As a result of mixing, a first mixed stream 222 having parameters as at a point 25 is formed. The mixed stream 222 having the parameters as at the point 25 passes through the heat exchanger HE1 where it is fully condensed and exits the heat exchanger HE1 as a first condensed stream 224 having parameters as at a point 26. The condensed stream 224 having the parameters as at the point 26 corresponding to a state of saturated liquid has a substantially leaner composition (*i.e.*, a substantially lower concentration of a low-boiling component of the multi-component fluid) than the input vapor stream 210.

[0030] Thereafter, the first condensed stream 224 having the parameters at the point 26 is optionally

divided into two liquid sub-streams 226 and 228, having parameters as at points 28 and 29, respectively, at a splitter 230. The second liquid sub-stream 228 having the parameters at the point 29 is forwarded to a liquid port 232 of the scrubber SC1. The first liquid sub-stream 226 is mixed with a second vapor stream 234 having parameters as at a point 27 from a vapor port 236 of the scrubber SC1 to form a second mixed stream 238 having parameters as at a point 30 at a second mixer 240. The second vapor stream 234 having the parameters as at the point 27 is in equilibrium or is in substantial equilibrium with the liquid sub-stream 226 having the parameters as at the point 28.

[0031] The second mixed stream 238 having the parameters as at the point 30 passes through the heat exchanger HE2 where the mixed stream 238 is fully condensed to form a second condensed stream 242 having parameters as at a point 31, corresponding to a state of saturated liquid. The saturated liquid of the second condensed stream 242 having the parameters as at the point 31 is always leaner (see above) than the input stream 210 having the parameters as at the point 21.

[0032] Thereafter, the second condensed stream 242 having the parameters as at the point 31 is divided into two liquid sub-streams 244 and 246, having parameters as at points 32 and 33, respectively, at a second splitter 248. Thereafter, the fourth liquid sub-stream 246 having the parameters as at the point 33 is mixed with a fourth vapor stream 250 having parameters as at a point 34, creating a third mixed stream 252 having parameters as at a point 35 at a third mixer 254. The composition of the third mixed stream 252 having the parameters as at the point 35 is the same or substantially the same as the composition of the input stream 210 that entered the system having the parameters as at the point 21. The third mixed stream 252 having parameters as at the point 35 passes through the heat exchanger HE3, where it is fully condensed to form an output condensed stream 256 having parameters as at a point 36 corresponding to a state of saturated liquid.

[0033] The vapor sub-stream 214 having parameters as at point 23 (as described above) is forwarded to a lower port 258 of the scrubber SC1, while the liquid stream 246 having the parameters as at the point 28 is sent into a top port 260 of the scrubber SC1. A counter flow process of mass and heat exchange occurs in the scrubber SC1, where liquid flows down the scrubber SC1 as vapor raises up. As a result, at the top of SC1, vapor is in equilibrium with liquid entering the top port 260 of the scrubber SC1. The resulting vapor exits the scrubber SC1 through an upper port 262 to form the vapor stream 250 having the parameters as at the point 34, which is mixed with the third liquid sub-stream 244 having the parameters as at the point 33 (as described above). Liquid collected at the bottom of SC1 is in equilibrium with vapor having the parameters as at the point 23 (as described



above) which has been sent to the bottom of the scrubber SC1. This liquid is removed from the scrubber SC1 via a bottom port 264 forming the first liquid stream 218 having the parameters as at the point 24, which is mixed with the vapor sub-stream 212 having the parameters as at the point 22 forming the first mixed stream 222 having the parameters as at the point 25 (as described above).

[0034] The vapor port 236 is located at an appropriate point in a middle region of the scrubber SC1, where the vapor stream 234 having the parameters as at the point 27 is removed, while the liquid port 232 is located at another appropriate point in a middle region of the scrubber SC1, where the liquid stream 228 having the parameters as at the point 29 is added. The interaction between these two streams 228 and 234 having the parameters 29 and 27, respectively, and the stream 224 having the parameters as at the point 26 is as described above.

[0035] The system is closed save for the input stream 210 and the output stream 256. Of course, when this condensing apparatus comprises a part of a complete energy extraction unit, the entire system is closed, *i.e.*, a multi-component fluid is sent through of vaporizing unit, then to an energy extraction unit and then to a fluid condensation unit of this invention and then back to the vaporizing unit forming a closed loop.

### **Three Heat Exchange Stages - One Scrubber - Second Embodiment**

[0036] Referring now to **Figure 3**, a preferred embodiment of a system for condensing a multi-component fluid, generally 300, is shown to comprise three heat exchange stages 302, 304, and 306, each stage including a heat exchanger HE1, HE2, and HE3, respectively. The system also includes a scrubber SC1. An input vapor stream 310 comprising a multi-component fluid (the stream to be condensed) and having initial parameters as at a point 41, which can correspond to a state of saturated vapor, enters the system 300. The stream 310 is divided into vapor two sub-streams 312 and 314, having parameters as at points 42 and 43, respectively, at a splitter 316. The first vapor sub-stream 312 having the parameters as at the point 42 is mixed with a first liquid stream 318 having parameters as at a point 44 at a mixer 320. The state of liquid in the first liquid stream 318 having the parameters as at the point 44 corresponds to a state of saturated liquid, which is in equilibrium with the saturated vapor sub-stream 312 having parameters as at the point 42. As a result of mixing, a first mixed stream 322 having parameters as at a point 45 is formed. The mixed stream 322 having the parameters as at the point 45 passes through the heat exchanger HE1 where it is fully condensed and exits the heat exchanger HE1 as a first condensed stream 324 having parameters as at a point 46. The condensed stream 324 having the parameters as at the point 46 corresponding to a state of saturated liquid has a substantially leaner composition (*i.e.*, a substantially lower concentration of

a low-boiling component of the multi-component fluid) than the input vapor stream 310.

[0037] Thereafter, the first condensed stream 324 having the parameters at the point 46 is optionally mixed with a liquid stream 328 having parameters as at a point 49 at a second mixer 330 to form a liquid stream 326, where the liquid stream 328 is withdrawn from the scrubber SC1 at a liquid port 332. The liquid stream 326 is then mixed with a second vapor stream 334 having parameters as at a point 47 from a vapor port 336 of the scrubber SC1 to form a second mixed stream 338 having parameters as at a point 50 at a second mixer 340. The second vapor stream 334 having the parameters as at the point 47 is in equilibrium or is in substantial equilibrium with the liquid sub-stream 326 having the parameters as at the point 48.

[0038] The second mixed stream 338 having the parameters as at the point 50 passes through the heat exchanger HE2 where the mixed stream 338 is fully condensed to form a second condensed stream 342 having parameters as at a point 51, corresponding to a state of saturated liquid. The saturated liquid of the second condensed stream 342 having the parameters as at the point 51 is always leaner (see above) than the input stream 310 having the parameters as at the point 41.

[0039] Thereafter, the second condensed stream 342 having the parameters as at the point 51 is divided into two liquid sub-streams 344 and 346, having parameters as at points 52 and 53, respectively, at a second splitter 348. Thereafter, the third liquid sub-stream 344 having the parameters as at the point 53 is mixed with a fourth vapor stream 350 having parameters as at a point 54, creating a third mixed stream 352 having parameters as at a point 55 at a third mixer 354. The composition of the third mixed stream 352 having the parameters as at the point 55 is the same or substantially the same as the composition of the input stream 310 that entered the system having the parameters as at the point 41. The third mixed stream 352 having parameters as at the point 55 passes through the heat exchanger HE3, where it is fully condensed to form an output condensed stream 356 having parameters as at a point 36 corresponding to a state of saturated liquid.

[0040] The vapor sub-stream 314 having parameters as at point 43 (as described above) is forwarded to a lower port 358 of the scrubber SC1, while the liquid stream 346 having the parameters as at the point 48 is sent into a top port 360 of the scrubber SC1. A counter flow process of mass and heat exchange occurs in the scrubber SC1, where liquid flows down the scrubber SC1 as vapor rises up. As a result, at the top of SC1, vapor is in equilibrium with liquid entering the top port 360 of the scrubber SC1. The resulting vapor exits the scrubber SC1 through an upper port 362 to form the vapor stream 350 having the parameters as at the point 54, which is mixed with the third liquid sub-stream 344 having the parameters as at the point 53 (as described above). Liquid collected at the

bottom of SC1 is in equilibrium with vapor having the parameters as at the point 43 (as described above) which has been sent to the bottom of the scrubber SC1. This liquid is removed from the scrubber SC1 via a bottom port 364 forming the first liquid stream 318 having the parameters as at the point 24, which is mixed with the vapor sub-stream 312 having the parameters as at the point 42 forming the first mixed stream 322 having the parameters as at the point 45 (as described above). [0041] The vapor port 336 is located at an appropriate point in a middle region of the scrubber SC1, where the vapor stream 334 having the parameters as at the point 47 is removed, while the liquid port 332 is located at another appropriate point in a middle region of the scrubber SC1, where the liquid stream 328 having the parameters as at the point 49 is added. The interaction between these two streams 328 and 334 having the parameters 49 and 47, respectively, and the steam 324 having the parameters as at the point 46 is as described above.

[0042] The system is closed save for the input stream 310 and the output stream 356. Of course, when this condensing apparatus comprises a part of a complete energy extraction unit, the entire system is closed, *i.e.*, a multi-component fluid is sent through of vaporizing unit, then to an energy extraction unit and then to a fluid condensation unit of this invention and then back to the vaporizing unit forming a closed loop.

#### **Four Heat Exchange Stages - One Scrubber**

[0043] Referring now to **Figure 4**, a preferred embodiment of a system for condensing a multi-component fluid, generally 400, is shown to comprise four heat exchange stages 402, 404, 406 and 408, each stage including a heat exchanger HE1, HE2, HE3 and HE4, respectively. The system also includes a scrubber SC1. A vapor multi-component stream 410, the stream to be condensed, and having initial parameters as at a point 61, which can correspond to a state of saturated vapor, enters the system 400. The initial vapor stream 410 is divided into two sub streams 412 and 414, having parameters as at points 62 and 63, respectively at a splitter 416. The vapor sub-stream 412 having the parameters as at the point 62 is mixed with a first liquid stream 418 having parameters as at a point 64 at a mixer 420. The state of liquid in the liquid stream 418 having parameters as at the point 64 corresponds to a state of saturated liquid, which is in equilibrium with the saturated vapor sub-stream 412 having parameters as at the point 62. As a result of mixing, a first mixed stream 422 having parameters as at a point 65 is formed. The mixed stream 420 having the parameters as at the point 65 passes through the heat exchanger HE1 where it is fully condensed and exits the heat exchanger HE1 as a first condensed stream 424 having parameters as at a point 66. The condensed stream 424 having the parameters as at the point 66 corresponding to a state of

saturated liquid having a substantially leaner composition (*i.e.*, a substantially lower concentration of a low-boiling component of the multi-component fluid) than the initial stream 410.

[0044] Thereafter, optionally a scrubber liquid stream 426 having parameters as at a point 69 is added to the condensed stream 424 having the parameters at the point 66, forming a first combined liquid stream 428 having parameters as at a point 68 at mixer 430. The parameters of the stream 426 are substantially the same, if not identical to the parameters of the stream 424. Alternatively, the first condensed stream 410 having the parameter as a the point 66 is split into liquid sub-streams 426 and 428 as at splitter 430, where the sub-stream 426 is sent to the scrubber SC1. The two optional alternatives are indicated by dashed lines with bi-directional arrows for stream 426 as shown in Figure 4. As the liquid stream 426 is optional, it is of course an alternative that no liquid is added or removed from the condensed stream 424 having the parameters as at the point 66. However, in all cases, we designate the stream 428 to have the parameter as at the point 68.

[0045] Thereafter, a scrubber vapor stream 432 having parameters as at point 67 is added to the stream 428 having parameters as the point 68 at a mixer 434, forming a mixed stream 436 having parameters as at a point 70. The vapor stream 432 having parameters as at point 67 is in equilibrium or is substantially in equilibrium with the liquid stream 428 having the parameters as at the point 68.

[0046] The stream 436 having the parameters as at the point 70 then passes through heat exchanger HE2 where it is fully condensed to form a second condensed stream 438 having parameters as at a point 71, corresponding to a state of saturated liquid. The saturated liquid of the condensed stream 438 is always leaner (see above) than the initial stream 410 having the parameters as at the point 61.

[0047] Similarly and optionally, a scrubber liquid stream 440 having parameters as at a point 74 is added to the condensed stream 438 having the parameters at the point 71, forming a second combined liquid stream 442 having parameters as at a point 73 at mixer 444. The parameters of the stream 440 are substantially the same, if not identical to the parameters of the stream 438. Alternatively, the second condensed stream 438 having the parameter as a the point 71 is split into liquid sub-streams 440 and 442 as at a splitter 444, where the sub-stream 440 is sent to the scrubber SC1. The two optional alternatives are indicated by dashed lines with bi-directional arrows for stream 440 as shown in Figure 4. As the liquid stream 440 is optional, it is of course an alternative that no liquid is added or removed from the condensed stream 438 having the parameters as at the point 71. However, in all cases, we designate the stream 442 to have the parameter as at the point 73.

[0048] Thereafter, a second scrubber vapor stream 446 having parameters as at point 72 is added

to the stream **442** having parameters as the point **73** at a mixer **448**, forming a second mixed stream **450** having parameters as at a point **75**. The vapor stream **446** having parameters as at point **72** is in equilibrium or is substantially in equilibrium with the liquid stream **442** having the parameters as at the point **73**.

[0049] The mixed stream **450** having the parameters as at the point **75** then passes through heat exchanger **HE3** where it is fully condensed to form a third condensed stream **452** having parameters as at a point **76**, corresponding to a state of saturated liquid. The saturated liquid of the condensed stream **452** is always leaner (see above) than the initial stream **410** having the parameters as at the point **61**.

[0050] Thereafter, the third condensed stream **452** having the parameters as at the point **76** is divided into two liquid sub-streams **454** and **456**, having parameters as at points **77** and **78**, respectively, at a fourth splitter **458**. Thereafter, the liquid sub-stream **456** having the parameters as at the point **78** is mixed with a third scrubber vapor stream **460** having parameters as at a point **79**, creating a fourth mixed stream **462** having parameters as at a point **80** at a third mixer **464**. The composition of the fourth mixed stream **462** having the parameters as at the point **80** is the same or substantially the same as the composition of the input stream **410** that entered the system having the parameters as at the point **61**. The fourth mixed stream **462** having parameters as at the point **80** passes through the fourth heat exchanger **HE4**, where it is fully condensed to form an output condensed stream **466** having parameters as at a point **81** corresponding to a state of saturated liquid.

[0051] The stream **414** of vapor of having parameters as at point **63** (as described above) is sent into a bottom port **468** of the scrubber **SC1**, while the liquid sub-stream **454** having parameters as at the point **77** is sent into a top port **470** of the scrubber **SC1**. A counter flow process of mass and heat exchange occurs in the scrubber **SC1**, where liquid flows down the scrubber **SC1** as vapor raises up. As a result, at the top of the scrubber **SC1**, vapor of the vapor stream **460** is in equilibrium with liquid of the liquid stream **454** having the parameters as at the point **77**, which was sent to the top port **470** of the scrubber **SC1** (see above). This vapor stream **460** having the parameters as at the point **79** is withdrawn from the scrubber at an upper port **472** and then mixed with the liquid stream **456** having the parameters as at the point **78** (as described above). Liquid collected at the bottom of **SC1** is in equilibrium with vapor in the vapor stream **414** having the parameters as at the point **63** (as described above) which entered the scrubber **SC1** at the bottom port **468**. This liquid is removed from the scrubber **SC1** at a bottom port **474** forming the liquid stream **418** having the parameters as at the point **64**, which was mixed with the vapor sub-stream **412** having the

parameters as at the point 26 forming the mixed stream 422 having the parameters as at the point 63 (as described above).

[0052] From appropriate ports 476 and 478, respectively, in a middle section of the scrubber SC1, optional liquid streams 426 and 440 are removed or added depending on the specific embodiment. From other appropriated ports 478 and 480, respectively, in a middle section of the scrubber SC1, the vapor streams 432 and 446 are removed. The liquid stream 426 and the vapor stream 432 are used to modify the stream 436 going into the second heat exchanger HE2 or the second heat exchanger HE2 and the scrubber SC1. Similarly, the liquid stream 440 and the vapor stream 446 are used to modify the stream 450 going into the third heat exchanger HE3 or the third heat exchanger HE3 and the scrubber SC1. One experienced in the art can always find a proper position of withdrawal and/or addition of streams 426, 432, 440, and 442.

[0053] The system is closed save for the input stream 410 and the output stream 466. Of course, when this condensing apparatus comprises a part of a complete energy extraction unit, the entire system is closed, *i.e.*, a multi-component fluid is sent through of vaporizing unit, then to an energy extraction unit and then to a fluid condensation unit of this invention and then back to the vaporizing unit forming a closed loop.

#### **Detailed Description of Two Scrubber Embodiment** **Three Heat Exchange Stages - Two Scrubber**

[0054] Referring now to Figure 5, a preferred embodiment of the condensation system of this, generally 500 is shown to comprise four heat exchange stages 502, 504, and 508, each stage including a heat exchanger HE1, HE2 and HE3, respectively. The system also includes two scrubbers SC1, and SC2, one for each of the intermediate heat exchangers HE1 and HE2. Because this embodiment represents a variation of the system of Figure 2, the stream are numbered accordingly with primes to distinguish the streams over the stream of Figure 2.

[0055] An input vapor stream 510 comprising a multi-component fluid (the stream to be condensed) and having initial parameters as at a point 21', which can correspond to a state of saturated vapor, enters the system 500. The stream 510 is divided into vapor two sub-streams 512 and 514, having parameters as at points 22' and 23', respectively, at a splitter 516. The first vapor sub-stream 512 having the parameters as at the point 22' is mixed with a first liquid stream 518 having parameters as at a point 24' at a mixer 520. The state of liquid in the first liquid stream 518 having the parameters as at the point 24' corresponds to a state of saturated liquid, which is in equilibrium with the saturated vapor sub-stream 512 having parameters as at the point 22'. As a result of mixing, a

first mixed stream **522** having parameters as at a point **25'** is formed. The mixed stream **522** having the parameters as at the point **25'** passes through the heat exchanger **HE1** where it is fully condensed and exits the heat exchanger **HE1** as a first condensed stream **524** having parameters as at a point **26'**. The condensed stream **524** having the parameters as at the point **26'** corresponding to a state of saturated liquid has a substantially leaner composition (*i.e.*, a substantially lower concentration of a low-boiling component of the multi-component fluid) than the input vapor stream **510**.

[0056] Thereafter, optionally a scrubber liquid stream **526** having parameters as at a point **29'** is added to the condensed stream **524** having the parameters at the point **26'**, forming a first combined liquid stream **528** having parameters as at a point **28'** at mixer **530**. The scrubber liquid stream **526** exits the scrubber **SC1** via liquid port **532**. The parameters of the stream **528** are substantially the same, if not identical to, the parameters of the stream **524**. Alternatively, the first condensed stream **524** having the parameter as at the point **26'** is split into liquid sub-streams **526** and **528** as at splitter **530**, where the sub-stream **526** is sent to the scrubber **SC1** at the port **532**. The two optional alternatives are indicated by dashed lines with bi-directional arrows for stream **526** as shown in Figure 5. As the liquid stream **526** is optional, it is of course an alternative that no liquid is added or removed from the condensed stream **524** having the parameters as at the point **26'**. However, in all cases, we designate the stream **528** to have the parameter as at the point **28'**.

[0057] The stream **528** is then mixed with a second vapor stream **534** having parameters as at a point **27'** from a vapor port **536** of the scrubber **SC1** to form a second mixed stream **538** having parameters as at a point **30'** at a second mixer **540**. The second vapor stream **534** having the parameters as at the point **27'** is in equilibrium or is in substantial equilibrium with the liquid sub-stream **526** having the parameters as at the point **28'**.

[0058] The second mixed stream **538** having the parameters as at the point **30** passes through the heat exchanger **HE2** where the mixed stream **538** is fully condensed to form a second condensed stream **542** having parameters as at a point **31'**, corresponding to a state of saturated liquid. The saturated liquid of the second condensed stream **542** having the parameters as at the point **31'** is always leaner (see above) than the input stream **510** having the parameters as at the point **21'**.

[0059] Thereafter, the second condensed stream **542** having the parameters as at the point **31'** is divided into two liquid sub-streams **544** and **546**, having parameters as at points **32'** and **33'**, respectively, at a second splitter **548**. Thereafter, the fourth liquid sub-stream **446** having the parameters as at the point **33'** is mixed with a fourth vapor stream **550** having parameters as at a point **34'**, creating a third mixed stream **552** having parameters as at a point **35'** at a third mixer **554**.

The composition of the third mixed stream **552** having the parameters as at the point **35'** is the same or substantially the same as the composition of the input stream **510** that entered the system having the parameters as at the point **21'**. The third mixed stream **552** having parameters as at the point **35'** passes through the heat exchanger **HE3**, where it is fully condensed to form an output condensed stream **556** having parameters as at a point **36'** corresponding to a state of saturated liquid.

[0060] The vapor sub-stream **514** having parameters as at point **23'** (as described above) is forwarded to a lower port **558** of the scrubber **SC1**, while the liquid stream **544** having the parameters as at the point **32'** is sent into a top port **560** of the scrubber **SC1**. A counter flow process of mass and heat exchange occurs in the scrubber **SC1**, where liquid flows down the scrubber **SC1** as vapor raises up. As a result, at the top of **SC1**, vapor is in equilibrium with liquid entering the top port **560** of the scrubber **SC1**. The resulting vapor exits the scrubber **SC1** through an upper port **562** to form an inter-scrubber vapor stream **564** having parameters as at a point **37'**, which is forwarded to a lower port **566** of the second scrubber **SC2**. Liquid collected at the bottom of **SC1** is in equilibrium with vapor having the parameters as at the point **23'** (as described above) which has been sent to the bottom of the scrubber **SC1**. This liquid is removed from the scrubber **SC1** through a bottom port **568** forming the inter-scrubber liquid stream **570** having the parameters as at the point **38'**, which is forwarded to a top port **572** of the second scrubber **SC2**. A counter flow process of mass and heat exchange occurs in the second scrubber **SC2** as is true from the scrubber **SC1**, where liquid from the inter-scrubber stream **570** flows down the second scrubber **SC2** as vapor raises up from inter-scrubber vapor stream **564**. As a result, at the top of the second scrubber **SC2**, vapor is in equilibrium with liquid entering the top port **572** of the second scrubber **SC2**. The resulting vapor exits the second scrubber **SC2** through an upper port **574** to form the vapor stream **550** having the parameters of the point **34'**. Liquid collected at the bottom of the second scrubber **SC2** is in equilibrium with vapor having the parameters as at the point **37'** (as described above) which has been sent to the bottom of the second scrubber **SC2**. This liquid is removed from the second scrubber **SC2** through a bottom port **576** forming the liquid stream **518** having the parameters as at the point **24'**.

[0061] The vapor port **536** is located at an appropriate point in a middle region of the scrubber **SC1**, where the vapor stream **534** having the parameters as at the point **27'** is removed, while the liquid port **532** is located at another appropriate point in a middle region of the scrubber **SC1**, where the liquid stream **526** having the parameters as at the point **29'** is added or removed. The interaction between these two streams **526** and **534** having the parameters **29'** and **27'**, respectively, and the



steam 524 having the parameters as at the point 26' is as described above.

[0062] The system is closed save for the input stream 510 and the output stream 556. Of course, when this condensing apparatus comprises a part of a complete energy extraction unit, the entire system is closed, *i.e.*, a multi-component fluid is sent through of vaporizing unit, then to an energy extraction unit and then to a fluid condensation unit of this invention and then back to the vaporizing unit forming a closed loop.

[0063] As shown in Figures 1-4, the total process of condensation is divided into heat exchange stages, with a minimum of two heat exchange stages being the lower limit and the upper limit being as many heat exchange stages as desired, in which case intermediate addition and/or withdrawal streams from the scrubber SC1 (analogous to steams 226 and 234) are added to the middle heat exchange stages, excluding the first and last heat exchange stages. As an alternative, it is also possible to have a separate scrubber for each heat exchange section as shown in Figure 5. In such a case, liquid from the bottom of each scrubber must be sent to the top of the next scrubber (with lower average temperature). One experienced in the art will be able to design, upon this basis, an appropriate system for any specific need.

[0064] As can be seen from the presented description, in every heat exchange section of the heat exchanger, the process of condensation is a process of complete (*i.e.*, final) condensation, and therefore the heat transfer coefficient in these heat exchanger section is the highest possible for the condensation of multi-component fluids. This allows a significant reduction of the required surface, size and cost of these heat exchangers (or heat exchanger sections). The additional cost associated with the installation of a scrubber and the required piping is much less than the savings achieved by the increased heat transfer coefficient achievable in the heat exchange sections.

#### **Energy Extraction Apparatus Including a Condensation Apparatus of This Invention**

[0065] Referring now to Figure 6, a preferred embodiment of the condensation system of this, generally 600, is shown is shown is shown to include a multi-component working fluid vaporization unit 602. The unit 602 includes an heat source input 604 and a heat source output 606, where the input 604 inputs a heat source 608 shown here as an input heat source stream, but can be any other heat source and where the output 606 outputs a spent heat source 610 shown here as a spent heat source stream. Of course, if the heat source was focused sun light or other forms of electromagnetic radiation, then the input 604 would input light and the output 606 would output unused light.

[0066] The unit 602 also includes a liquid multi-component working fluid input 612 and a vapor multi-component working fluid output 614, where the liquid input 612 inputs an input liquid multi-

component working fluid stream 616 and where the vapor output 614 outputs a final vapor multi-component working fluid stream 618. The vapor stream 618 is forwarded to an energy conversion unit 620 through a conversion unit vapor input 622. The energy conversion unit 620 extracts thermal energy from the final vapor stream 618 to produce a spent stream 624 and useable energy such as electrical energy or the like. Such energy conversion units can include any energy conversion unit known in the art including those described in United States Pat. Nos.: 4,346,561; 4,489,563; 4,548,043; 4,586,340; 4,604,867; 4,674,285; 4,732,005; 4,763,480; 4,899,545; 4,982,568; 5,029,444; 5,095,708; 5,440,882; 5,450,821; 5,572,871; 5,588,298; 5,603,218; 5,649,426; 5,754,613; 5,822,990; 5,950,433; 5,953,918; and 6,347,520; in co-pending United States Pat. Appln. Ser. Nos.: 10/242,301 filed 12 September 2002; 10/252,744 filed 23 September 2002; 10/320,345 filed 16 December 2002, and 10/357,328 filed 03 February 2003, incorporated herein by reference.

[0067] The spent stream 624 exits the conversion unit 620 through a conversion output 626 and enters a multi-component working fluid condensation unit 628 of this invention through a condensation unit output 630. The condensation unit 628 fully condenses the spent stream 624 as set forth above forming the liquid stream 616 exiting from a condensation unit output 632, which then enters the vaporization unit 602 through the input 612 forming a closed loop system.

[0068] All references cited herein are incorporated by reference. While this invention has been described fully and completely, it should be understood that, within the scope of the appended claims, the invention may be practiced otherwise than as specifically described. Although the invention has been disclosed with reference to its preferred embodiments, from reading this description those of skill in the art may appreciate changes and modifications that may be made which do not depart from the scope of the invention as described above and claimed hereafter.